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IN THE CLAIMS:

Please amend the claims, as follows:

1. (Currently amended): A process of making a bleached mechanical wood pulp comprising:

providing an aqueous slurry of mechanical wood pulp;

~~providing an aqueous bleaching mixture consisting essentially of water and hydrogen peroxide;~~

~~providing an aqueous magnesium hydroxide slurry consisting essentially of water and magnesium hydroxide;~~

~~combining together the aqueous slurry of mechanical wood pulp, the aqueous slurry consisting essentially of magnesium hydroxide with and a the aqueous bleaching mixture consisting essentially of hydrogen peroxide and magnesium hydroxide, to form a bleaching pulp mixture, the bleaching pulp mixture being at having a pH of from about 5.0 to 8.5, and the magnesium hydroxide having an initial concentration in the bleaching pulp mixture of at least about 0.5 wt. %, based on pulp dry mass; and~~

~~bleaching the bleaching pulp mixture for a time sufficient to produce the bleached mechanical wood pulp, the bleached mechanical wood pulp having an ISO brightness of up to about 75%, and the magnesium hydroxide having a BET surface area of about 7 to about 15 m²/g.~~

2. (Original) A process according to claim 1, wherein the bleaching mixture also comprises up to about 0.5 wt. % based on pulp dry mass of a chelating agent.

3. (Original) A process according to claim 2, wherein the chelating agent is selected from the group consisting of diethylenetriaminepentaacetic acid, ethylenediaminetetraacetic acid, N-(2-hydroxyethyl) ethylenediaminetriacetic acid, diethylenetriamine pentamethylene phosphonic acid, cyclic ethers, and their salts, and mixtures thereof.

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4. (Original) A process according to claim 3, wherein the chelating agent is diethylenetriaminepentaacetic acid.
5. (Original) A process according to claim 1, wherein the bleaching pulp mixture is maintained for a reaction time of up to about 6 hours.
6. (Original) A process according to claim 1, wherein the bleaching pulp mixture is heated so as to be maintained at a temperature range of about 120 °F to about 210 °F.
7. (Original) A process according to claim 1, wherein the hydrogen peroxide has an initial concentration in the bleaching pulp mixture of up to about 6 wt. %, based on pulp dry mass.
8. (Original) A process according to claim 7, wherein the hydrogen peroxide has an initial concentration of about 1 to about 6 wt. % based on pulp dry mass.
9. (Previously presented): A process according to claim 1, wherein the magnesium hydroxide has an initial concentration in the bleaching pulp mixture of from about 0.5 wt. % up to about 5 wt. %, based on pulp dry mass.
10. (Currently amended): A process according to claim 9, wherein the magnesium hydroxide has an initial concentration of from about ± 0.5 up to about 2 wt. % based on pulp dry mass in the bleaching pulp mixture.
11. (Currently amended): A process according to claim 1, wherein the bleaching mixture magnesium hydroxide contains less than about 250 ppm Mn, less than about 0.15 wt. % Fe, and less than about 250 ppm Cu, based on the equivalent mass of Mg(OH)₂.

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12. (Previously presented): A process according to claim 1, wherein the bleaching pulp mixture has a final pH of about 6.5 to about 8.0.

13. (Previously presented): A process according to claim 1, wherein the bleached wood pulp has an ISO brightness of more than about 65 %.

14. (Currently amended): A process according to claim 1, wherein the initial ratio of magnesium hydroxide to hydrogen peroxide in said bleaching mixture is about 25 parts to about 75 parts of magnesium hydroxide to about 100 parts of hydrogen peroxide, based on a $\text{Mg}(\text{OH})_2$ chemical equivalence.

15. (Cancelled).

16. (Currently Amended): A process of making a bleached mechanical wood pulp comprising:

providing an aqueous slurry of mechanical wood pulp;

~~adding providing a first chelating agent to said mechanical wood pulp;~~

providing ~~a an~~ aqueous bleaching mixture consisting essentially of water and hydrogen peroxide;

~~and providing an aqueous magnesium hydroxide slurry consisting essentially of water and magnesium hydroxide;~~

~~combining the aqueous slurry of mechanical wood pulp, the first chelating agent, with the aqueous bleaching mixture, and the aqueous magnesium hydroxide slurry to form a bleaching pulp mixture, the bleaching pulp mixture being at a pH of from about 5.0 to 8.5, and the magnesium hydroxide having an initial concentration in the bleaching pulp mixture of at least about 0.5 wt. %, based on pulp dry mass; and~~

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~~washing the mechanical wood pulp, and optionally dewatering the slurry to form a washed mechanical wood pulp;~~

~~combining the washed mechanical wood pulp with said bleaching mixture; and bleaching the bleaching pulp mixture for a time sufficient to produce the bleached mechanical wood pulp, the bleached mechanical wood pulp having an ISO brightness of up to about 75%, and the magnesium hydroxide having a BET surface area of about 7 to about 15 m²/g.~~

17. (Original) A process according to claim 16, wherein the first chelating agent comprises up to about 0.5 wt. %, based on pulp dry mass, of diethylenetriaminepentaacetic acid, ethylenediaminetetraacetic acid, N-(2-hydroxyethyl) ethylenediaminetriacetic acids, diethylenetriamine pentamethylene phosphonic acid, cyclic ethers, and their salts.

18. (Original) A process according to claim 16, wherein the bleaching mixture comprises up to about 0.5 wt. %, based on pulp dry mass, of a second chelating agent, said second chelating agent being added at a different point in the process than said first chelating agent.

19. (Original) A process according to claim 18, wherein said first chelating agent is added to said pulp, and said second chelating agent is added to said bleaching pulp mixture or to said bleaching mixture prior to mixing with said pulp.

20. (Original) A process according to claim 19, wherein the second chelating agent is selected from the group of diethylenetriaminepentaacetic, ethylenediaminetetraacetic acid, N-(2-hydroxyethyl) ethylenediaminetriacetic acids, diethylenetriamine pentamethylene phosphonic acid, cyclic ethers, and their salts, and mixtures thereof.

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21. (Original) A process according to claim 20, wherein the first and second chelating agents are diethylenetriaminepentaacetic acid.
22. (Original) A process according to claim 16, wherein the bleaching pulp mixture is maintained for a reaction time of up to about 6 hours.
23. (Original) A process according to claim 16, wherein the bleaching pulp mixture is heated so as to be maintained at a temperature range of about 120 °F to about 210 °F.
24. (Original) A process according to claim 16, wherein the hydrogen peroxide has an initial concentration in the bleaching pulp mixture of up to about 6 wt. %, based on pulp dry mass.
25. (Original) A process according to claim 24, wherein the hydrogen peroxide has an initial concentration of about 1 to about 6 % based on pulp dry mass.
26. (Previously presented): A process according to claim 24, wherein the magnesium hydroxide has an initial concentration of about 0.5 to about 5.0 wt. % based on pulp dry mass in the bleaching pulp mixture.
27. (Previously presented): A process according to claim 16, wherein the ~~magnesium~~ hydroxide contains less than about 250 ppm Mn, less than about 0.15 wt. % Fe, and less than about 250 ppm Cu, based on the equivalent mass of $Mg(OH)_2$.
28. (Previously presented): A process according to claim 16, wherein the bleaching pulp mixture has a final pH of about 6.5 to about 8.0.

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29. (Previously presented): A process according to claim 16, wherein the bleached wood pulp has an ISO brightness of more than about 65 %.

30. (Currently amended): A process according to claim 16, wherein the initial ratio of magnesium hydroxide to hydrogen peroxide in said bleaching mixture is about 25 parts to about 75 parts of hydroxide to about 100 parts hydrogen peroxide, ~~based on a $\text{Mg}(\text{OH})_2$ chemical equivalence.~~

31. (Cancelled).

32. (Currently Amended): A process of making a bleached mechanical wood pulp comprising:

providing an aqueous slurry of mechanical wood pulp;

~~providing an aqueous bleaching mixture consisting essentially of water, and hydrogen peroxide;~~

~~providing an aqueous magnesium hydroxide slurry consisting essentially of water and magnesium hydroxide;~~

~~combining the aqueous slurry of mechanical wood pulp, with a the aqueous bleaching mixture, and the aqueous consisting essentially of hydrogen peroxide and magnesium hydroxide slurry, to form a bleaching pulp mixture, the bleaching pulp mixture being at having a pH of from about 5.0 to 8.5, and the magnesium hydroxide having an initial concentration in the bleaching pulp mixture of at least about 0.5 wt. %, based on pulp dry mass;~~

~~bleaching the bleaching pulp mixture for a time sufficient to produce the bleached mechanical wood pulp, the bleached mechanical wood pulp having an ISO brightness of up to about 75%, and the magnesium hydroxide having a BET surface area of about 7 to about 15 m^2/g ;~~

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separating the bleached mechanical wood pulp from a filtrate comprising water and residual hydrogen peroxide; and

recycling at least a portion of said filtrate as at least a portion of said bleaching pulp mixture.

33. (Original) A process according to claim 32, wherein the bleaching pulp mixture also comprises up to 0.5 wt. % of a chelating agent, based on pulp dry mass.

34. (Original) A process according to claim 33, wherein the chelating agent is selected from the group consisting of diethylenetriaminepentaacetic acid, ethylenediaminetetraacetic acid, N-(2-hydroxyethyl) ethylenediaminetriacetic acid, diethylenetriamine pentamethylene phosphonic acid, cyclic ethers, their salts, and mixtures thereof.

35. (Original) A process according to claim 34, wherein the chelating agent is diethylenetriaminepentaacetic acid.

36. (Original) A process according to claim 32, wherein the bleaching pulp mixture is maintained for a reaction time of up to about 6 hours.

37. (Original) A process according to claim 32, wherein the bleaching pulp mixture is heated so as to be maintained at a temperature range of about 120 °F to about 210 °F.

38. (Original) A process according to claim 32, wherein the hydrogen peroxide has an initial concentration in the bleaching pulp mixture of up to about 6 wt. %, based on pulp dry mass.

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39. (Original) A process according to claim 38, wherein the hydrogen peroxide has an initial concentration of about 1 to about 6 wt. % based on pulp dry mass.

40. (Currently amended): A process according to claim 32, wherein the magnesium hydroxide has an initial concentration in the bleaching pulp mixture of from about 0.5 wt. % up to about 5 wt. %, based on pulp dry mass.

41. (Currently amended): A process according to claim 40, wherein the magnesium hydroxide has an initial concentration of from about ± 0.5 to about 2 wt. % based on pulp dry mass.

42. (Previously presented): A process according to claim 32, wherein the magnesium hydroxide contains less than about 250 ppm Mn, less than about 0.15 wt. % Fe, and less than about 250 ppm Cu, based on the equivalent mass of $\text{Mg}(\text{OH})_2$.

43. (Previously presented): A process according to claim 32, wherein the bleaching pulp mixture has a final pH of about 6.5 to about 8.0.

44. (Previously presented): A process according to claim 32, wherein the bleached wood pulp has an ISO brightness of more than about 65 %.

45. (Currently amended): A process according to claim 32, wherein the initial ratio of magnesium hydroxide to hydrogen peroxide in said bleaching mixture is about 25 parts to about 75 parts of magnesium compound hydroxide per about 100 parts of hydrogen peroxide, based on a $\text{Mg}(\text{OH})_2$ chemical equivalence.

46. (Cancelled)

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47. (Original) A process according to claim 32, wherein fresh hydrogen peroxide is added to said filtrate prior to recycle as bleaching mixture.

48. (Original) A process according to claim 32, wherein at least a portion of said filtrate and said bleaching mixture are combined prior to combining with said wood pulp.

49. (Previously presented): A process according to claim 1, wherein the mechanical wood pulp is selected from a group consisting of stone groundwood (SGW), pressurized stone groundwood (PSGW), refiner mechanical (RMP) and thermomechanical pulp (TMP).

50. (Previously presented): A process according to claim 16, wherein the mechanical wood pulp is selected from a group consisting of stone groundwood (SGW), pressurized stone groundwood (PSGW), refiner mechanical (RMP) and thermomechanical pulp (TMP).

51. (Previously presented): A process according to claim 16, wherein the mechanical wood pulp is selected from a group consisting of stone groundwood (SGW), pressurized stone groundwood (PSGW), refiner mechanical (RMP) and thermomechanical pulp (TMP).

52. (Previously presented): A process according to claim 1, wherein bleaching pulp mixture is formed in the absence of sodium silicate.

53. (Previously presented): A process according to claim 16, wherein bleaching pulp mixture is formed in the absence of sodium silicate.

54. (Previously presented): A process according to claim 32, wherein bleaching pulp mixture is formed in the absence of sodium silicate.

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55. (Previously presented): A process according to claim 1, wherein bleaching pulp mixture is formed in the absence of sodium hydroxide.

56. (Previously presented): A process according to claim 16, wherein bleaching pulp mixture is formed in the absence of sodium hydroxide.

57. (Previously presented): A process according to claim 32, wherein bleaching pulp mixture is formed in the absence of sodium hydroxide.

58. (Cancelled)

59. (Cancelled)

60. (Cancelled)